Mathematical Modeling of Disc Type Winding of Power Transformer

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Abstract- In order to achieve this network modeling method was studied and network model for the said winding type was understood. A MATLAB programme was written with top down approach to solve hydraulic and thermal network of the said winding. A simplified heat conduction model was developed and implemented in MATLAB code for prediction of hot spot in a conductor of a disc. The coupled thermo-hydraulic network model studied was then implemented in a simple MATLAB code that used functions to solve hydraulic network, thermal network and conductor heat conduction model.

Keyword - Transformer winding, Mathematical model, CFD, Network modelling, MATLAB code.

I. INTRODUCTION

A device was designed and perfected over several decades in 19th century by several of European and American engineers that used principals of electromagnetic induction for voltage manipulations. It was called Transformer. By the end of 19th century 3 phase transformers had came to existence in its form that is used till date. A power transformer is the electrical device which is used to change the voltage of AC in power transmission system. The first transformer in the world was invented in 1840s. Modern large and medium power transformers consist of oil tank with oil filling in it, the cooling equipment on the tank wall and the active part inside the tank. As the key part of a transformer, the active part consists of 2 main components: the set of coils or windings (at least comprising a low voltage, high voltage and a regulating winding) and the iron core. For a step-up transformer, the primary coil is low voltage (LV) input and the secondary coil is high voltage (HV) output. The situation is opposite for a stepdown transformer. The iron core is the part inducing the varying magnitude flux. Nowadays, transformers play key roles in long distance high-voltage power transmission.

II. NETWORK MODELING AND DEVELOPMENT OF MATLAB CODE

Methodology

The methodology implemented in aforementioned research paper authored by Oliver A.J. (1980) [8]is described in following section

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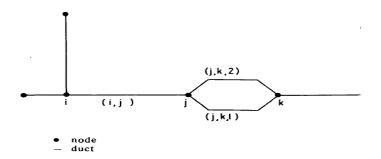


Fig.1.1 Simple network diagram

A collection of interconnecting flow paths or ducts can be represented on the network diagram of the type shown in Figure 1.1 Each element of the network represents a single path with the nodes usually being placed at the junctions. In the model, values of the pressure and bulk temperature are determined for each node. Values of fluid velocity and average wall temperature are determined for each path. If the temperature varies significantly along a path, then that path could be split into several elements in order to calculate this variation.

The required values of pressure, bulk temperature, fluid velocity and wall temperature are obtained by solving the set of equations which can be obtained from the following:

- a. conservation of mass applied to each node
- b. conservation of thermal energy applied to each node
- c. pressure-drop equation applied to each path
- d. heat-transfer equation applied to each path.

The actual equations and the method of solution are discussed in later section.

Solution Procedure

The following assumptions were made in deriving the equations:

- Flow in ducts is assumed 1D laminar (Re < 200)
- Oil is completely mixed at junction i.e. all branches leaving node have same Thermodynamic state.
- Hydraulically developed boundary layer i.e. uniform velocity along length of duct
- Pure convective heat transfer with developing thermal boundary layer i.e. linearly increasing temperature profile along length of duct
- Uniform heat flux at each surface of duct

The set of equations which are obtained from (a) to (d) in preceding Section are given below.

Application of the conservation of mass to a node i, see Figure 1.1, gives

$$\sum_{\substack{j=1\\i\neq i}}^{M} \alpha_{i,j} \sum_{l=1}^{m_{i,j}} \rho_{i,j} u_{i,j} A_{i,j} = -\dot{m}_i$$
 (1)

where, $\sum \alpha_{i,j}$ represents all the paths which connect nodes j to node i. Where $\alpha_{i,j}$ is connection matrix for flow network.

Its value is,

- +1 if flow is from node j to i
- -1 if flow is from node *i to j*

0 if node j and i are not connected

 $\sum_{l}\{term\}$ allows for more than one path between a node i and a node j. The case of l>1 can be handled by the solution procedure, but to simplify the equations it will be assumed for the rest of this Section that two nodes i and j are directly connected by only one path (i.e. l=1). In this case eqn. 4.1 reduces to

$$\sum_{\substack{j=1\\j\neq i}}^{M} \alpha_{i,j} \rho_{i,j} u_{i,j} A_{i,j} = -\dot{m}_i$$
 (2)

The pressure drop equation for a path (i, j) joining nodes i and j can be expressed as

where term I represents the losses which are related to the velocity head, for example friction; terms II and III are the losses which are proportional to the velocity head in another pipe, these could occur at junctions; term IV represents the gravitational head; term V allows for any pressure sources (pumps) or sink.

These equations form a complete set for the network considered. Their solution provides values of pressure, P_i , and bulk temperature $(t_b)_i$ at each node and values of velocity, $u_{i,j}$, and mean wall temperature $(t_w)_{i,j}$ for each duct.

Friction Facto

CFD calibrated correlation for friction factor is given formulated in aforementioned research paper authored by Wu W. et al. (2012) [21] is given below.

$$f = \frac{24}{Re} \left[0.17 Re^{0.37} Pr^{0.15} \left(\frac{L}{D} \right)^{-0.55} \left(\frac{\mu_w}{\mu_b} \right)^{0.9} + 0.61 \right]$$
(4)

Junction Pressure Loss Coefficient:

Coefficients of equation for the junction pressure loss equations in Tee junction presented in research paper authored by Jamison were corrected using CFD. The corrected correlations are as follows:

For Junction Pressure Loss in confluence,

$$\Delta P_{a \to m} = K_{a \to m} \times \frac{1}{2} \rho u_m^2$$
Where a is 1 or 2

$$K_{1\to m} = 0.03 \left(1 - \frac{\dot{V}_1}{\dot{V}_m}\right)^2$$

$$- \left(\frac{\dot{V}_1}{\dot{V}_m}\right)^2 \left\{1 + \left(\frac{\cos \theta}{a} - 1\right) \left(1.62 - (r)^{1/2}\right) 0.38(1 - a)\right\}$$

$$+ \frac{\dot{V}_1}{\dot{V}_m} (2 - a) \left(1 - \frac{\dot{V}_1}{\dot{V}_m}\right)$$
 (b)

$$\begin{split} K_{2 \to m} &= \, -0.92 \left(1 - \frac{\dot{V}_2}{\dot{V}_m} \right)^2 \\ &- \left(\frac{\dot{V}_2}{\dot{V}_m} \right)^2 \left\{ \left(\frac{\cos \theta}{a} - 1 \right) \left(1.2 - (r)^{1/2} \right) \right\} \\ &+ 0.4 \left(\frac{\dot{V}_2}{\dot{V}_m} \right)^2 \left(\frac{1}{a} - 1 \right) \cos \theta \\ &+ \frac{\dot{V}_2}{\dot{V}_m} (2 - a) \left(1 \right) \\ &- \frac{\dot{V}_2}{\dot{V}_m} \right) \end{split}$$

The notation used to identify each branch at junction in equations of junction pressure losses is given shown in fig. 1.2

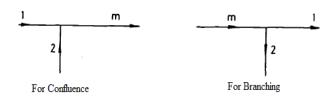


Fig. 1.2 Notation used for junction losses

Nusselt number

Heat transfer in rectangular duct with laminar oil flow regime was studied by CFD and Nusselt corrected Nusselt number equation was presented as follows.

$$Nu = 1.29 \left(\frac{L_{/D}}{RePr}\right)^{-0.38} \left(\frac{\mu_W}{\mu_D}\right)^{-0.16} + 3.08$$
 (5)

Boundary values

For any flow network problem, a pressure must be specified at one node at least. Furthermore for a node i with a mass source it is necessary to either

(i) specify \dot{m}_i and $(t_b)_i$

or

(ii) specify P_i and $(t_b)_i$

and for a node j with a mass sink then either

(iii) specify \dot{m}_i

(iv) specify P_i

For winding network condition (i) and (iv) were used

Fig. shows vertical section of the disc with as many conductors as there are turns in the disc. In a disc Heat is generated at every location along the length of conductor cable but heat dissipation to transformer oil takes place only from top and bottom surfaces as well as inner and outer walls on circumference of disc. Heat conduction along the length of conductor that is in circumferential direction is assumed to be negligible. Fig. shows enlarged view of individual conductor section and its heat interactions at boundary.

Node C represent the shaded region which is cross section of conductor. Node N, E, S and W represent the top, right, bottom and left wall of conductor-insulation cross section respectively. $Q_{\text{gen,c}}$ is rate of heat generation at the Node C in W/m. The Heat generated dissipates through 4 walls at the boundary of conductor-insulation section by conduction. Thus Q_{CN} , Q_{CE} , Q_{CS} and Q_{CW} represent conductive heat transfer from Node C to Node N, E, S and W respectively.

Thus from conservation of energy,

$$Q_{CN} + Q_{CE} + Q_{CS} + Q_{CW} = Q_{gen,c}$$
 (6)

Conduction heat transfer between Node C an N can be represented by,

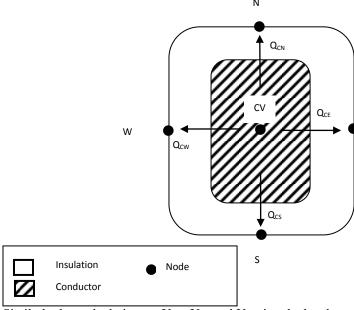
$$Q_{CE} = Y_{CE}(T_C - T_E) \tag{7}$$

Where Y_{CW} is thermal admittance of composite section of conductor and insulation material between Node C and Node ES.

T_C is conductor temperature and T_E is temperature of

Thus
$$Y_{CE} = \frac{1}{\left(\frac{K_{ins.}(d_c + 2d_p)}{d_p} + \frac{K_{cond.}d_c}{0.5b - d_p}\right)} {\left(\frac{(d_c + 2d_p)}{0.5b}\right)}$$
 (8)

Where K_{ins.} and K_{cond.} are thermal conductivity of insulation and conductor material respectively.



Similarly thermal admittance Y_{CN} , Y_{CS} and Y_{CW} is calculated. By substituting Eq. 3.16 in 3.15,

$$Y_{CN}(T_C - T_N) + Y_{CE}(T_C - T_E) + Y_{CS}(T_C - T_S) + Y_{CW}(T_C - T_W) = Q_{gen,c}$$
(9)

To solve Equation for conductor temperature T_C; T_N, T_E, T_S and Tw should be known in priory. In the analysis of winding network disc wall temperatures are obtained as mentioned in 'Methodology'. Thus for all conductors in a disc temperature at Node N and S is known but temperature at nodes E and W are unknown except for end conductors where temperature of one more node is known which is in contact with oil duct. In order to eliminate the unknown terms in equation conservation of energy is applied to Node on wall of conductor interfacing conductor 1 and 2.

$$Y_{C1X}(T_{C1} - T_X) = -Y_{C2X}(T_{C2} - T_X)$$
 (10)
Where X is W or E

Since all conductor-insulation sections are identical

$$Y_{C1X} = Y_{C2X}$$

Hence $T_X = \frac{T_{C1} + T_{C2}}{2}$ (11)

Substituted in equation for n conductors in a disc. The set of equation is expressed as,

$$\begin{split} & \left\{ \sum_{k} Y_{pk} - \sum_{k} \frac{Y_{pk}(1-\beta_{pk})}{2} \right\} T_{p} + \\ & \left[\sum_{k} \left\{ \frac{(-1)Y_{pk}(1-\beta_{pk})Y_{pk}(1-Y_{pk})}{4} \right\} \right] T_{p-1} + \\ & \left[\sum_{j} \left\{ \frac{Y_{pk}(1-\beta_{pk})Y_{pk}(1+Y_{pk})}{4} \right\} \right] T_{p+1} = \\ & Q_{gen,p} + \sum_{k} Y_{pk}\beta_{pk}T_{k} \quad for \ p = 1 \to n \quad (12) \\ & \text{Where } k \text{ is } \{ \text{N, S, E, W} \} \end{split}$$

 β_{nk} is 0 if temperature at node k of conductor p is unknown and 1 if otherwise

is +1 if conductor p shares node k with conductor p+1is -1 if conductor p shares node k with conductor p-1 is 0 otherwise

Dimensions of investigated geometry, material properties and excitation condition $\$

The pass example is from a disc-type winding and the studied section is between two neighbouring spacers, as shown in Fig. 1.4.

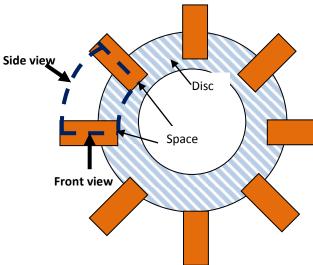


Fig. 1.4 Studied Section of Winding Geometry

There are 8 discs in the pass; they are cooled with oil which flows in from the bottom inlet, through horizontal channels between the rows of 'heat generating' discs, and joins up with a single vertical channel at the opposite side that carries the oil upwards and through a gap to next pass. The next pass starts from the oil block washer equipped just below the 9th disc; all washers are assumed as fully tight.

Comparison of results

The results for oil flow distribution in studied winding pass in research paper authored by Weinlader A. et al. (2012) [24] are presented in graphical form. Mass flow rate in each horizontal duct of pass is normalized as follows.

% MFR (Mass flow rate) =
$$\frac{\text{Mass flow rate duct}}{\text{Inlet Mass flow rate}} \times 100$$

Ducts are numbered from bottom to top.

Fig. 1.5, 1.6 and 1.7 compares % MFR in ducts predicted by case 1, 2 and present network model for inlet oil flow rate of 2 lit/min, 10 lit/min and 20 lit/min respectively. The comparison for inlet mass flow rate of 5 lit/min and 15 lit/min is not shown here.

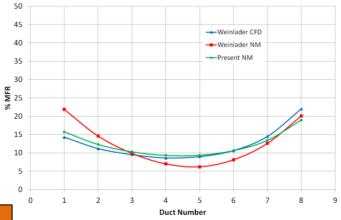


Fig. 1.5 Comparison of %MFR vs Duct number for 2 lit/min.

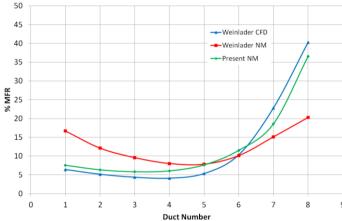


Fig. 1.6 Comparison of %MFR vs Duct number for 10 lit/min.

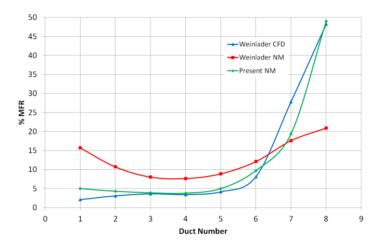


Fig. 1.6 Comparison of %MFR vs Duct number for 20 lit/min.

CONCLUSION

Use of CFD in the analysis of cooling duct design of disc type winding with oil guiding washers yields thorough understanding of heat interactions and flow patterns of oil in winding but it requires high computational efforts. Network modeling is developed and used for transformer in thermal analysis of disc type winding since 1980s' which is well balanced between calculation speed and accuracy of results. To obtain general idea of flow pattern and fair estimates of temperature distribution in winding development of

mathematical tool based on network modeling was summoned in Crompton Greaves Ltd which is one of the major international manufacturers of power transformer.

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